

Figure 3 is a plot of conversion versus time for  $\text{NO}_x$  and  $\text{C}_3\text{H}_8$ , corresponding to Comparative Example 9.

B<sup>2</sup> cont'd 13.--  
Figure 4 is a plot of conversion versus time for  $\text{NO}_x$  and  $\text{C}_3\text{H}_8$ , corresponding to Example

In the Claims

B<sup>3</sup> 12. (Twice amended) The  $\text{NO}_x$  reducing catalyst according to Claim 11, wherein the crystalline metallosilicate has the average diameter for the [primary particle] crystal size of 0.01 to 0.2  $\mu\text{m}$ .

B<sup>4</sup> 4. (Once amended) The  $\text{NO}_x$  reducing catalyst according to Claim 3, wherein the crystalline metallosilicate is of BEA [type] structure.

10. (Twice amended) The process for reducing  $\text{NO}_x$  according to Claim 6, wherein the catalyst essentially consists of the crystalline metallosilicate, which is BEA [type] structure aluminosilicate with an  $\text{SiO}_2/\text{Al}_2\text{O}_3$  ratio of 10 to 100 and ion-exchanged with Co to have a Co/Al ratio between 0.2 and 0.6.

B<sup>5</sup> 11. (Twice amended) The process for reducing  $\text{NO}_x$  according to Claim 16, wherein the catalyst essentially consists of BEA [type] structure aluminosilicate in which a part of Si is substituted by Ti, and/or a part of Al is substituted by B, and which is ion-exchanged with Co to have a Co/Al ratio between 0.2 and 0.6.

F 12. (Once amended) The process for reducing  $\text{NO}_x$  according to Claim 11, wherein the catalyst essentially consists of BEA [type] structure aluminosilicate with an  $\text{SiO}_2/\text{Al}_2\text{O}_3$  ratio between 10 and 100 and with an  $\text{SiO}_2/\text{TiO}_2$  ratio between 20 and 200.

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15. (Once amended) A catalyst for reducing nitrogen oxides (NO<sub>x</sub>) with hydrocarbons in an oxygen-rich atmosphere, comprising crystalline metallosilicate ion-exchanged with Co, said crystalline metallosilicate having a plurality of straight channels of oxygen [8-ring] 10-ring or larger in section, said plurality of straight channels being oriented in at least two different dimensional directions, individual members of said plurality of straight channels communicating with each other via micropores having a size of oxygen 8-ring or larger[, the straight channels oriented in at least one of said at least two different dimensional directions having a size in section of oxygen 10-ring or larger].

16. (Once amended) A process for reducing NO<sub>x</sub> in exhaust gas, which contains hydrocarbons and excess oxygen, by hydrocarbons having two or larger number of carbons, comprising the step of: contacting the exhaust gas with a catalyst which contains at least crystalline metallosilicate ion-exchanged with Co, said crystalline metallosilicate having a plurality of straight channels of oxygen [8-ring] 10-ring or larger in section, said plurality of straight channels being oriented in at least two different dimensional directions, individual members of said plurality of straight channels communicating with each other via micropores having a size of oxygen 8-ring or larger[, the straight channels oriented in at least one of said at least two different directions having a size in section of oxygen 10-ring or larger].

18. (Once amended) A process for reducing NO<sub>x</sub> by hydrocarbons in exhaust gas containing hydrocarbons and excess oxygen, in which 50% more of hydrocarbons calculated in terms of methane are methane, comprising: contacting the exhaust gas with a catalyst that at least contains BEA [type] structure aluminosilicate with an SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> ratio between 10 and 100 and with an SiO<sub>2</sub>/B<sub>2</sub>O<sub>3</sub> ratio before ion exchange between 20 and 500, and is ion-exchanged with Co to have a Co/Al ratio between 0.2 and 0.6.